

Motivation and Objectives

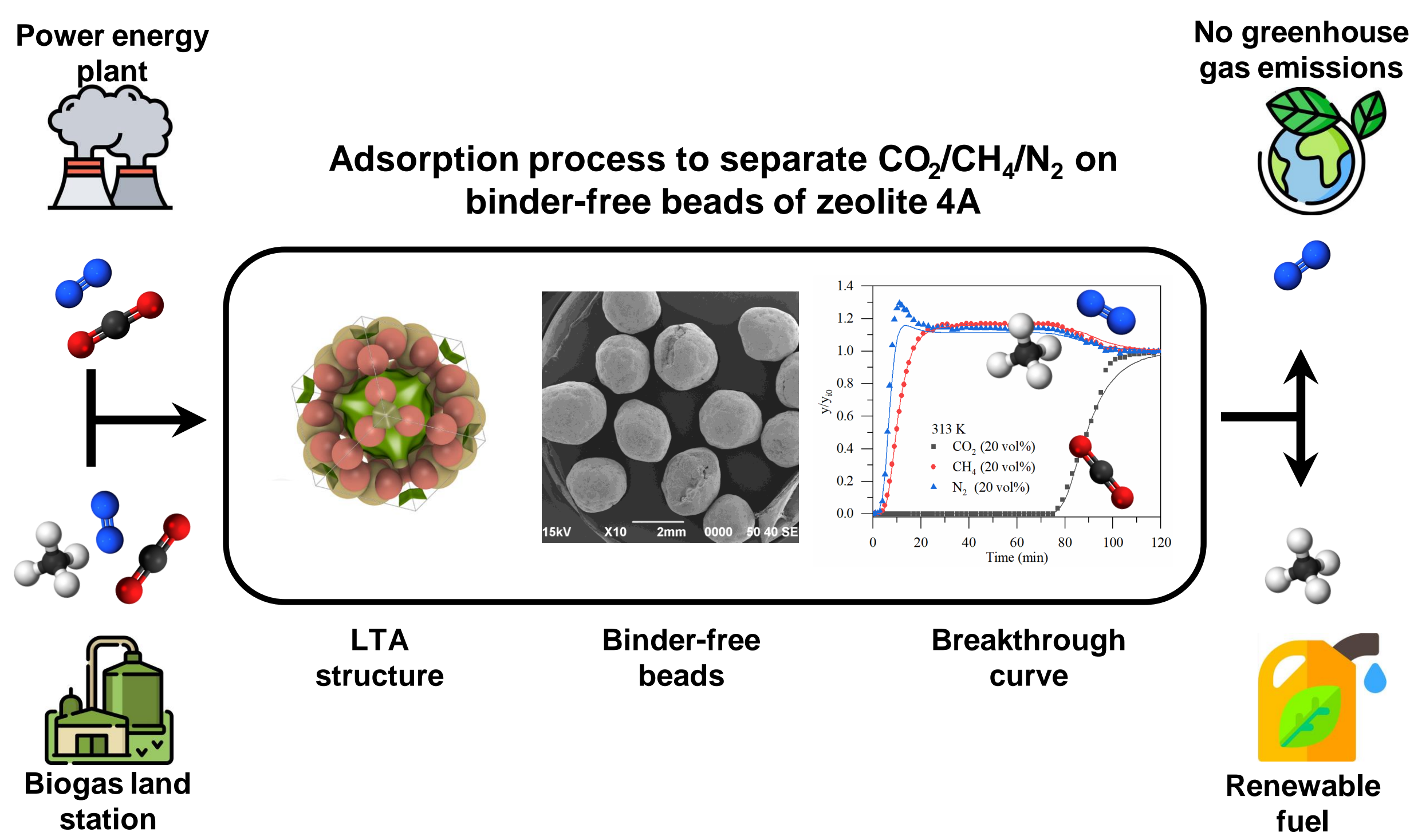
The presence of CO₂ (40 vol.%) in the biogas composition can reduce its calorific value, impairs its transport via pipelines, and, consequently, limits its use [1]. CO₂ released from coal-fired power plants has been contributing to a massive 73% of annual emissions for the energy sector [2]. In this way, this work seeks to evaluate the separation of CO₂, CH₄, and N₂ on binder-free zeolite 4A in conditions of interest to biogas upgrading and CO₂ capture from the post-combustion stream.



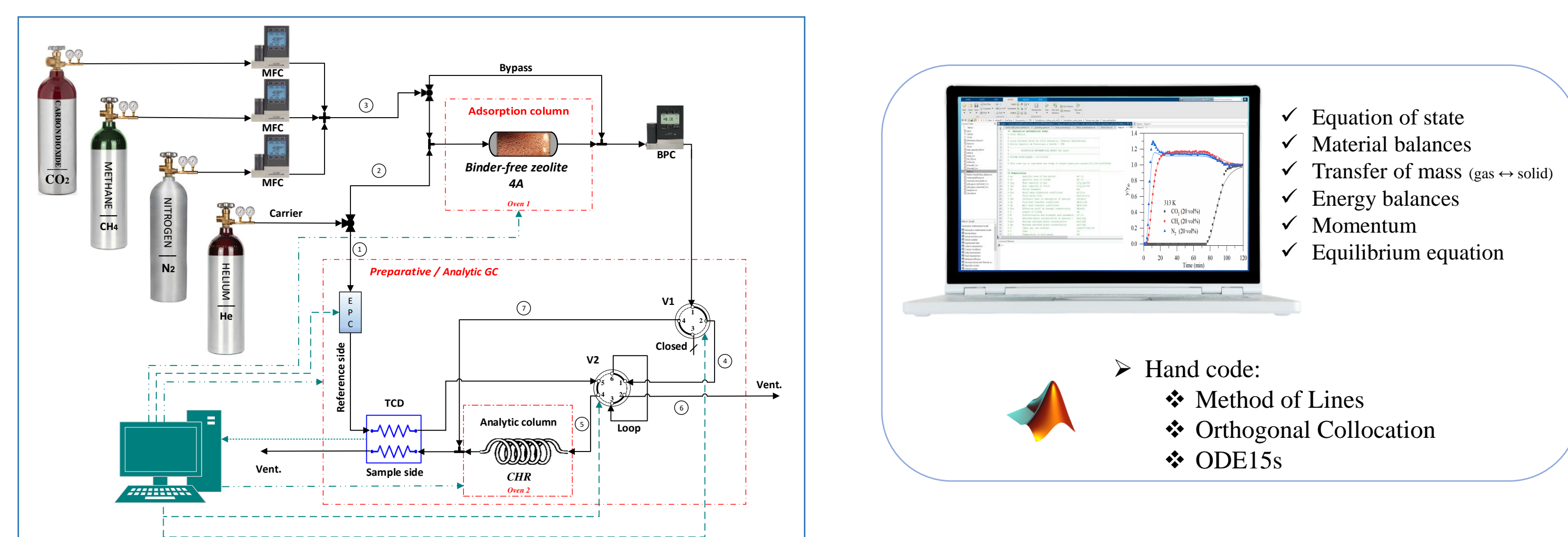
Evaluate the binder-free zeolite 4A (BF4A) to separate CO₂, CH₄, and N₂.



Increase knowledge on equilibrium and dynamic interaction between BF4A and CO₂, CH₄, and N₂.



Methodology



$$q^* = \frac{q_{m1,i} b_{1i} p_i}{1 + b_{1i} p_i} + \frac{q_{m2,i} b_{2i} p_i}{1 + b_{2i} p_i}$$

$$\alpha_{AB} = \left(\frac{q_A^*}{y_A} \right) / \left(\frac{q_B^*}{y_B} \right)$$

* Experiments performed at 313, 373, and 423 K and up to 3.5 bar.

Conclusions and Future Work

- Binder-free zeolite 4A act as an efficient separator of CO₂ from CH₄ and N₂
- Selectivities to CO₂ around 72 over N₂ and 38 over CH₄
- Dual-site Langmuir and Standard Langmuir described well the equilibrium data
- Mathematical model predicted well the breakthrough experiments

Ongoing/Future work: development of a conceptual pressure swing adsorption to evaluate the performance of binder-free zeolite 4A to address the biogas upgrading and CO₂ capture from post-combustion streams.

Equilibrium

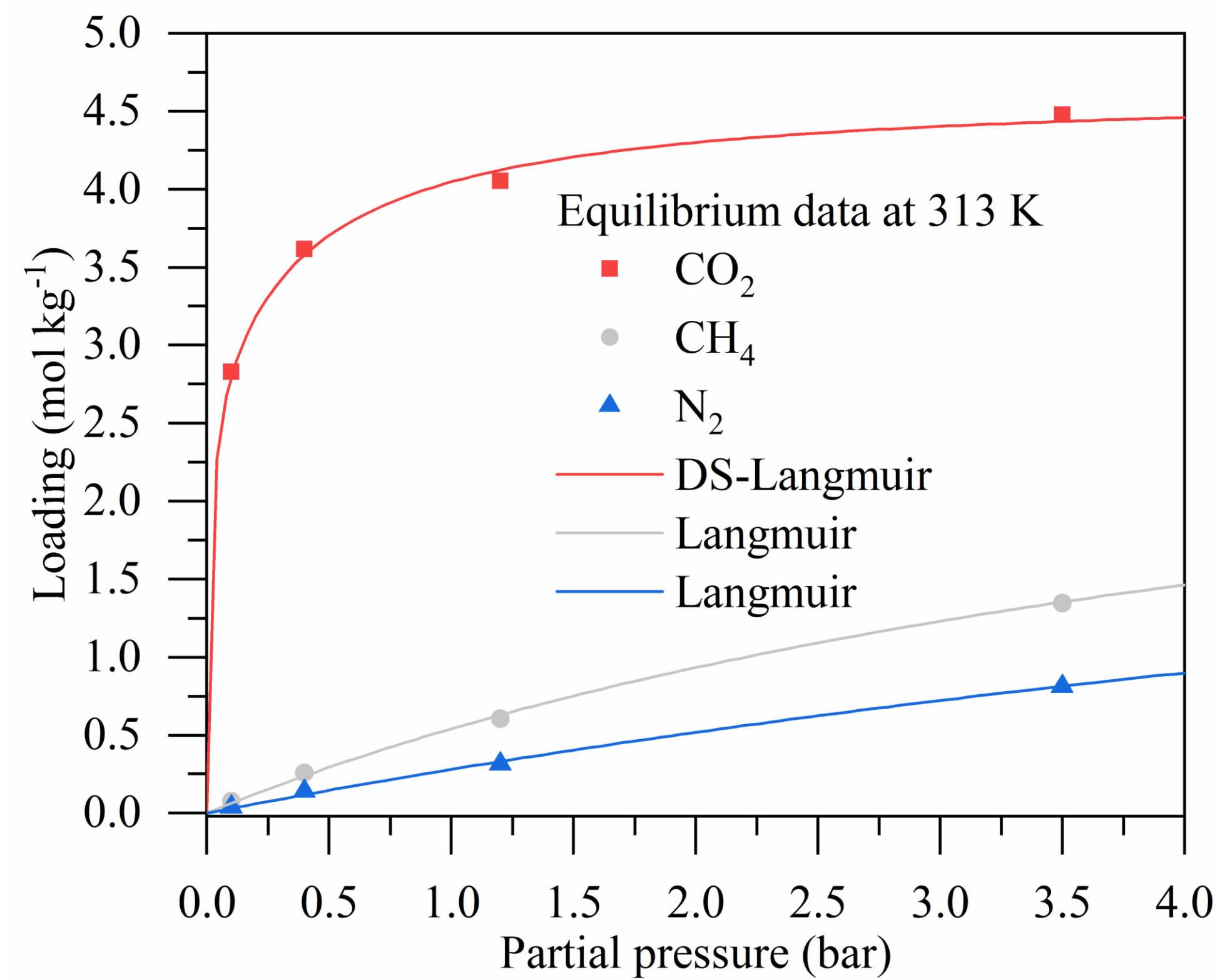


Fig. 1 – Equilibrium data of CO₂, CH₄, and N₂ on BF4A.

- At 313 K and 3.5 bar: CO₂ (4.48 mol/kg) > CH₄ (1.35 mol/kg) > N₂ (0.81 mol/kg)
- Isotherm shape: CO₂ (highly nonlinear), CH₄ (linear), N₂ (linear)
- Isotherm model: Dual-site Langmuir (CO₂), Langmuir (CH₄ and N₂)
- Equilibrium data well described by isotherm model

Kinetic Study

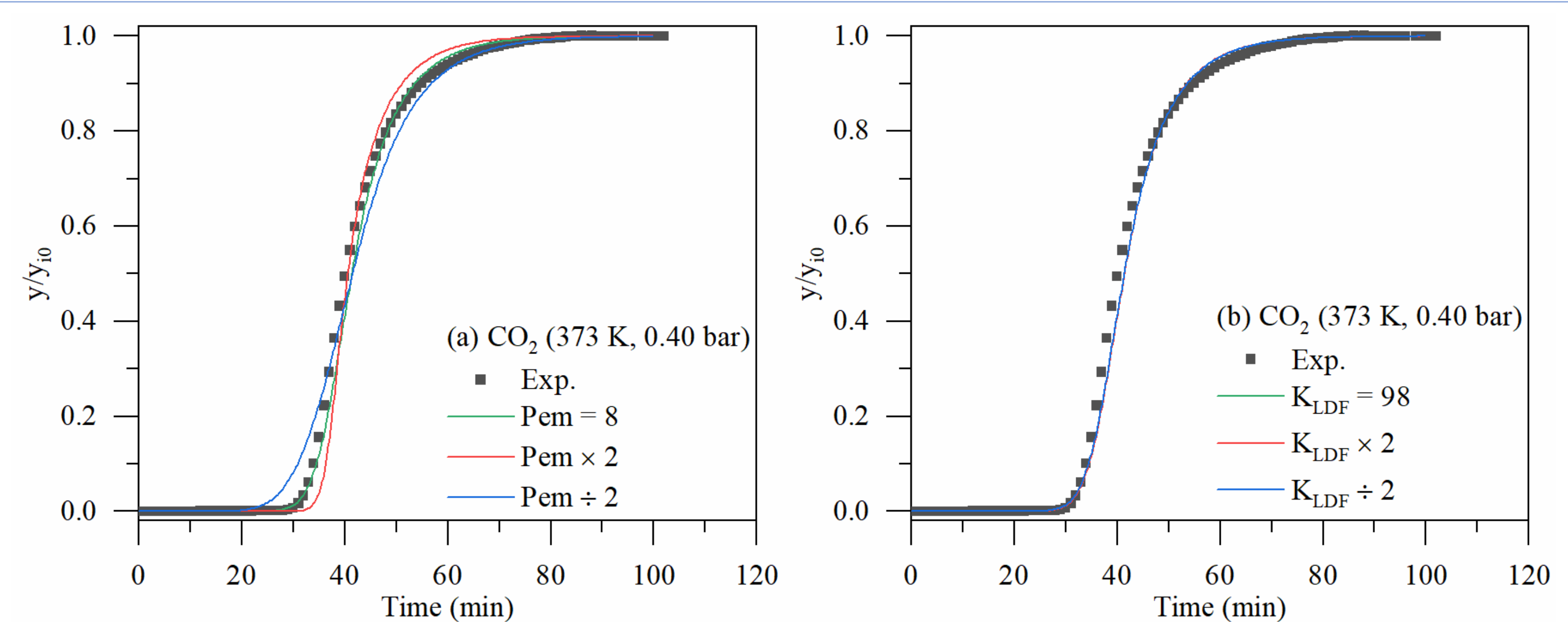


Fig. 2 – Effect of (a) axial Peclet number, and (b) overall mass transfer coefficient (K_{LDF}), on BF4A.

Peclet number

$$P_{em} = \frac{uL}{D_{ax}}$$

Lumped mass transfer

$$\frac{1}{K_{LDF}} = \frac{R_p}{3k_f} + \frac{R_p^2}{15\epsilon_p D_p} + \frac{r_c^2}{15K_d}$$

- The zone spreading in the fixed bed is completely dominated by axial dispersion

Dynamic separation and Selectivity

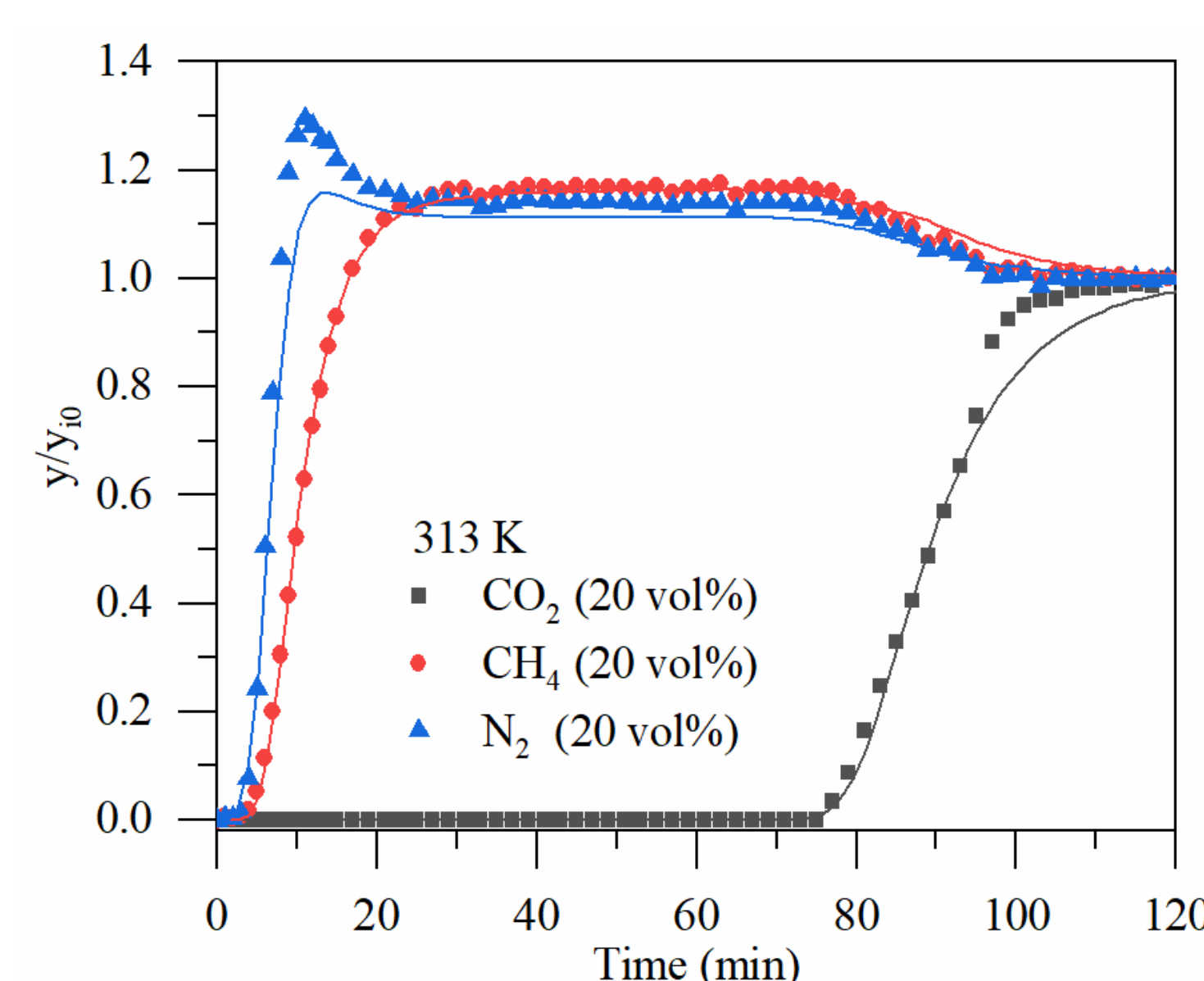


Fig. 3 – Ternary breakthrough of a mixture CO₂/CH₄/N₂ on BF4A at 5 bar.

Selectivity post-combustion condition*:

$$\alpha_{CO_2, N_2} = 72$$

Selectivity biogas condition**:

$$\alpha_{CO_2, CH_4} = 38$$

- BF4A completely separates CO₂ from a mixture of CO₂/CH₄/N₂
- High selectivity towards CO₂ for two targets of application

* CO₂/N₂:15/85 vol.% at 1 bar and 313 K – predicted using extended isotherm (DS-Langmuir)
** CO₂/CH₄:33/67 vol.% at 1 bar and 313 K – predicted using extended isotherm (DS-Langmuir)

References and Acknowledgments

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References.

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